

PLI / GB 04 / 02863



INVESTOR IN PEOPLE

The Patent Office
Concept House
Cardiff Road
Newport

South Wales 20 JUL 2004
NP10 8QQ

WIPO

PCT

PRIORITY DOCUMENT

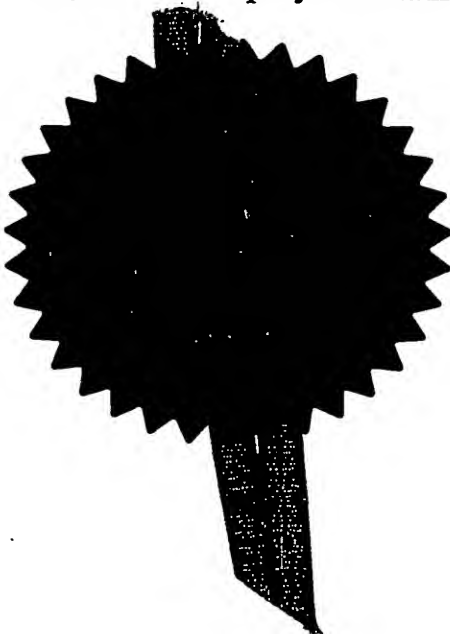
SUBMITTED OR TRANSMITTED IN
COMPLIANCE WITH RULE 17.1(a) OR (b)

I, the undersigned, being an officer duly authorised in accordance with Section 74(1) and (4) of the Deregulation & Contracting Out Act 1994, to sign and issue certificates on behalf of the Comptroller-General, hereby certify that annexed hereto is a true copy of the documents as originally filed in connection with the patent application identified therein.

In accordance with the Patents (Companies Re-registration) Rules 1982, if a company named in this certificate and any accompanying documents has re-registered under the Companies Act 1980 with the same name as that with which it was registered immediately before re-registration save for the substitution as, or inclusion as, the last part of the name of the words "public limited company" or their equivalents in Welsh, references to the name of the company in this certificate and any accompanying documents shall be treated as references to the name with which it is so re-registered.

In accordance with the rules, the words "public limited company" may be replaced by p.l.c., plc, P.L.C. or PLC.

Re-registration under the Companies Act does not constitute a new legal entity but merely subjects the company to certain additional company law rules.



Signed

Andrew

Dated

12 July 2004

THE PATENT OFFICE

12 AUG 2003

NEWPORT

The
Patent
Office12AUG03 E829492-1 D02831
F01/7700 0.00-0318840.6**Request for grant of a patent***(See the notes on the back of this form. You can also get an explanatory leaflet from the Patent Office to help you fill in this form)*

The Patent Office

Cardiff Road
Newport
South Wales
NP9 1RH

1. Your reference

57.0551 GB NP

2. Patent application number

(The Patent Office will fill in this part)

12 AUG 2003

0318840.6

3. Full name, address and postcode of the or of each applicant *(underline all surnames)*

M-I L.L.C.

5950 North Course Drive
Houston, Texas 77072
United States of AmericaPatents ADP number *(if you know it)*

If the applicant is a corporate body, give the country/state of its incorporation

Delaware, United States of America

8092132001

4. Title of the invention

Electrical treatment for oil based drilling or completion fluids

5. Name of your agent *(if you have one)*"Address for service" in the United Kingdom to which all correspondence should be sent *(including the postcode)*Akram MIRZA
Intellectual Property Law Department
Schlumberger Cambridge Research Limited
High Cross
Maddingley Road
Cambridge CB3 0EL
United Kingdom

4433504003

Patents ADP number *(if you know it)*6. If you are declaring priority from one or more earlier patent applications, give the country and the date of filing of the or of each of these earlier applications and *(if you know it)* the or each application number

Country

Priority application number
*(if you know it)*Date of filing
(day / month / year)

7. If this application is divided or otherwise derived from an earlier UK application, give the number and the filing date of the earlier application

Number of earlier application

Date of filing
*(day / month / year)*8. Is a statement of inventorship and of right to grant of a patent required in support of this request? *(Answer 'Yes' if:*

YES

- a) any applicant named in part 3 is not an inventor, or
 - b) there is an inventor who is not named as an applicant, or
 - c) any named applicant is a corporate body.
- See note (d))

Patents Form 1/77

9. Enter the number of sheets for any of the following items you are filing with this form. Do not count copies of the same document...

Continuation sheets of this form	-
Description	20
Claim(s)	2
Abstract	1
Drawing(s)	5

+5 PM

10. If you are also filing any of the following, state how many against each item.

Priority documents	-
Translations of priority documents	-
Statement of inventorship and right to grant of a patent (Patents Form 7/77)	1
Request for preliminary examination and search (Patents Form 9/77)	1
Request for substantive examination (Patents Form 10/77)	1
Any other documents (please specify)	-

11. I/We request the grant of a patent on the basis of this application.

Signature

Date

11 August 2003

12. Name and daytime telephone number of person to contact in the United Kingdom
- Akram MIRZA
01223 325268

Warning

After an application for a patent has been filed, the Comptroller of the Patent Office will consider whether publication or communication of the invention should be prohibited or restricted under Section 22 of the Patents Act 1977. You will be informed if it is necessary to prohibit or restrict your invention in this way. Furthermore, if you live in the United Kingdom, Section 23 of the Patents Act 1977 stops you from applying for a patent abroad without first getting written permission from the Patent Office unless an application has been filed at least 6 weeks beforehand in the United Kingdom for a patent for the same invention and either no direction prohibiting publication or communication has been given, or any such direction has been revoked.

Notes

- If you need help to fill in this form or you have any questions, please contact the Patent Office on 0645 500505.
- Write your answers in capital letters using black ink or you may type them.
- If there is not enough space for all the relevant details on any part of this form, please continue on a separate sheet of paper and write "see continuation sheet" in the relevant part(s). Any continuation sheet should be attached to this form.
- If you have answered 'Yes' Patents Form 7/77 will need to be filed.
- Once you have filled in the form you must remember to sign and date it.
- For details of the fee and ways to pay please contact the Patent Office.

DIPLOMA

ELECTRICAL TREATMENT FOR OIL BASED DRILLING OR COMPLETION
FLUIDS

Field of the Invention

The present invention relates to an electrical treatment for
oil based drilling or completion fluids.

Background

In the process of rotary drilling a well, a drilling fluid or
mud is circulated down the rotating drill pipe, through the
bit, and up the annular space between the pipe and the
formation or steel casing, to the surface. The drilling
fluid performs different functions such as removal of
cuttings from the bottom of the hole to the surface, to
suspend cuttings and weighting material when the circulation
is interrupted, control subsurface pressure, isolate the
fluids from the formation by providing sufficient hydrostatic
pressure to prevent the ingress of formation fluids into the
wellbore, cool and lubricate the drill string and bit,
maximise penetration rate etc.

The required functions can be achieved by a wide range of
fluids composed of various combinations of solids, liquids
and gases and classified according to the constitution of the
continuous phase mainly in two groupings: aqueous drilling
fluids, and oil based drilling fluids.

Aqueous fluids are the most commonly used drilling fluid
type. The aqueous phase is made up of fresh water or, more
often, of a brine. As discontinuous phase, they may contain
gases, water-immiscible fluids such as diesel oil which form
an oil-in-water emulsion, and solids including clays and

weighting material such as barite. The properties are typically controlled by the addition of clay minerals, polymers and surfactants.

5 In drilling water-sensitive zones such as reactive shales, production formations, or where bottom hole temperature conditions are severe or where corrosion is a major problem, oil based drilling fluids are preferred. The continuous phase is typically a mineral or synthetic oil which may be alkenic, olefenic, esteric etc. Such fluids also commonly
10 contain water or brine as discontinuous phase to form a water-in-oil or invert emulsion. Generally they furthermore contain a solid phase, which is essentially similar to that of aqueous fluids, and additives for the control of density, rheology and fluid loss. The invert emulsion is formed and
15 stabilised with the aid of one or more specially selected emulsifiers.

Oil based drilling fluids also typically contain oil-soluble surfactants that facilitate the incorporation of water-wet clay or non-clay formation minerals, and hence enable such
20 minerals to be transported to surface equipment for removal from circulation before the fluid returns to the drillpipe and the drillbit. The largest formation particles are rock cuttings, of size typically larger than 0.1 - 0.2 mm, removed by shale-shaker screens at the surface. Smaller particles,
25 typically larger than about 5 μ m, will pass through the screens, but can be removed by centrifuge.

Oil based drilling fluids have been used for many years, and their application is expected to increase, partly owing to their several advantages over water based drilling fluids,

but also owing to their ability to be re-used and re-cycled, so minimizing their loss and their environmental impact.

As mentioned above, during drilling, formation particles become incorporated into the drilling fluid. Unless these are removed, they eventually move the fluid's properties, particularly the rheological parameters, out of the acceptable range. However, formation particles that are colloidal in size (less than about 5 μm) are more difficult to remove than the larger particles. A longer centrifuge run-time would be sufficient to remove the colloidal particles if the fluid were merely viscous, but the quiescent drilling fluid is usually required to behave as a gel to support cuttings in periods without circulation. Such a fluid will have a gel strength, and will behave as a non-Newtonian, shear-thinning fluid in which the viscosity at low shear rates is very large compared with the viscosity at the circulation rate.

Gel strengths typical of oil based fluids (1 -10 Pa) can be shown to support particles of less than a few microns in size indefinitely against the centrifugal force typical of oilfield centrifuges, which then have no effect regardless of the time they run. Further, owing to their large specific surface area, colloidal-sized particles have a disproportionate effect on the rheology of a fluid.

Moreover, as more colloidal particles become part of the fluid, the gel strength will generally increase. Thus as more colloidal particles are incorporated in the drilling fluid, the upper particle size that can be supported by the gel, and hence unremoved by the centrifuge, also increases. Increasing quantities of colloidal particles are detrimental

to other aspects of a fluid's performance, particularly those engineering parameters important for efficient drilling.

Thus, in practice, the process of increasing colloidal concentration and decreasing treatment efficiency tends to continue until engineering parameters depart from their acceptable ranges. In particular, both the engineering rheology parameters PV and YP (API 1988) must be kept within bounds for efficient drilling. As drilling proceeds, and possibly also as the fluid is moved from one job to another, the driller can eventually find that PV and YP increase beyond their upper limits until the fluid becomes unusable for drilling and untreatable by centrifuge.

Typically PV should be in the range 20 to 100, and YP should lie between 15 to 55. Strictly, the PV and YP of drilling fluids are defined by the API-defined rheometer used to measure them, but they can be related to more generally used parameters by the Bingham Plastic rheology model in which the shear stress SS (in Pa) and shear rate SR (in reciprocal seconds or 1/s) are related by:

$$SS = BYS + BPV \times SR$$

where BYS is the Bingham yield stress in Pa and BPV is the Bingham plastic viscosity in Pa s. The oilfield unit YP as measured by the API method is given by $YP = 1.96 \times BYS(\text{Pa})$. Likewise, the oilfield unit PV = $1000 \times BPV(\text{Pa s})$.

Similar considerations apply to oil based completion fluids.

Summary of the Invention

In general terms, the present invention relates to an electrical treatment for oil based drilling or completion fluids whereby the particulate structure of the fluid and/or a filter cake or sedimentary bed formed from the fluid may be altered to give advantageous fluid, cake or bed properties. The drilling or completion fluids of the present invention generally have densities of at least 1100 kg/m^3 , and more preferably 1500 kg/m or 2000 kg/m .

One effect of applying a spatially uniform field, of e.g. 100 V mm^{-1} ; to an oil based fluid, is to cause charged colloidal particles to migrate to an electrode at which they concentrate and collect as a removable deposit. This phenomenon is well-known as electrophoresis (Delgado 2002), particularly in aqueous or highly-conductive fluids. US Patent No. 4,323,445 proposes an apparatus for electrokinetically separating water based drilling mud into liquid and solid phases. However, as far as we are aware, electrophoresis has not been exploited for the removal of colloidal or fine particles from oil based drilling or completion fluids, or any other similar non-aqueous application.

US 5,308,586 describes an electrostatic separator for removing very dilute fine particles from oils. However, in that application (i) the oil feed was relatively clean and free from the high concentrations of the weighting agents and emulsified brine typically found in drilling fluids, and (ii) the field was applied to the feed oil amongst a bed of glass beads.

Also it is known in the petroleum industry to apply very high electric fields for coalescing dispersed water droplets dispersed in oil (Thornton 1992, Eow et al. 2001). However, in general, the field strengths we propose are less than those at which emulsion droplets in an oil based drilling or completion fluid would coalesce to form continuous and electrically-conductive chains. Such fields, giving dielectric breakdown, are routinely measured in the API Electrical Stability Test (API 1988) for oil based drilling or completion fluids as a measure of emulsion stability and sufficiency of emulsifier.

Thus a first aspect of the present invention provides a method of removing particulate solids from an oil based drilling or completion fluid, comprising:

exposing the fluid to an electric field to electrically migrate particulate solids suspended therein, and collecting the migrated particulate solids to remove them from the fluid.

Typically, but not exclusively, the drilling or completion fluid comprises a water-in-oil emulsion. For such a fluid, the amount of water (in terms of the water to oil volume ratio) may be at least 5:95, and more preferably at least 30:70 or 50:50. The strength of the electric field is preferably lower than that required to coalesce the water droplets of the emulsion. The water generally contains a dissolved salt, i.e. the water is a brine.

Preferably, the strength of the electric field is less than 100,000 V/m, more preferably it is less than 10,000 V/m.

Preferably, the strength of the electric field is greater than 10 V/m, more preferably it is greater than 100 V/m.

5 In certain embodiments, the electric field is substantially uniform. However, in other embodiments the electric field is spatially non-uniform. One effect of non-uniform fields is well-known as dielectrophoresis (Pohl 1978) whereby the field induces an electric dipole moment in an uncharged particle of different electrical permittivity from the surrounding liquid. The particle is then caused by the field gradient to
10 migrate towards the high-field region where it can be collected. An advantage of the use of a non-uniform field is, therefore, that the migrating particles are not required to possess an electrical charge.

15 The PV and/or YP of the drilling or completion fluid is typically reduced as a result of the collection of the particulate solids.

Generally, the fluid contains clay particles and/or weighting agent (e.g. barite) particles.

20 The particulate solids in the fluid may occupy at least 5 vol. % and preferably at least 15 vol. % of the total fluid.

The drilling or completion fluid may be a shear-thinning fluid which forms a gel when quiescent. Thus the method allows colloidal particles to be removed from such a fluid.

25 The method may further comprise heating the fluid to enhance the collection of particulate solids. Preferably the fluid is heated to a temperature of at least 25°C, more preferably at least 50°C, and even more preferably at least 75°C.

A further aspect of the invention provides a method of recycling an oil based drilling or completion fluid by performing the method of the first aspect.

5 The method of recycling may include the step of using a centrifuge or hydrocyclone to remove other particulate solids from the fluid. This step may be performed before or after the electrical treatment.

Brief Description of the Drawings

10 The invention will now be described in more detail, with reference to the drawings in which:

Figure 1 shows schematically a simple electrophoretic separating assembly;

Figure 2 shows schematically an apparatus used for quantitative electrophoretic separating tests;

15 Figure 3 is a graph of mass of deposit against voltage;

Figure 4 shows a further graph of mass of deposit against voltage;

Figure 5 shows a graph of current against voltage;

Figure 6 shows a graph of deposit weight against rotor speed;

20 Figure 7 shows a graph of deposit weight against test temperature;

Figure 8 shows schematically a longitudinal section through a device for recycling oil based mud; and

Figures 9a and b respectively show longitudinal and transverse sections of an alternative device for recycling oil based mud.

Detailed Description

5 Tests have been performed on oil based drilling fluids in which a steady electrical field was applied to a sample of oil based mud to remove solid particles by depositing them on one electrode, leaving the drilling fluid depleted of such particles. In most cases the deposit was formed on the
10 negative electrode, which suggests that the particles were positively-charged, but the process is equally applicable to the treatment of fluids containing negatively-charged particles.

Drilling fluids

15 Initial tests were conducted with field samples in which the base oil was mineral oil. The field samples were a conventional invert emulsion based on a Versaclean™ oil based mud (OBM) formulation. These are tightly emulsified, temperature-stable, invert-emulsion, oil based drilling
20 fluids. The following components are found in such formulations: primary and secondary emulsifiers, blends of liquid emulsifiers, wetting agents, gellants, fluid stabilizing agents, organophilic clay (amine treated bentonite), CaCl_2 brine, filtration control additives and
25 barite as a weighting agent. The field sample drilling fluids were aged by circulation at geothermal temperatures, and contained some fine particles, typically clay, resulting from the drilling process.

Further tests were also conducted on field samples of a Versaport™ OBM system. The Versaport systems have elevated low shear rate viscosities. Versaport is either a conventional or relaxed filtrate system, the relaxed filtrate system comprising: primary emulsifier, surfactant, oil-wetting agents, lime, viscosifiers and gelling agents, organophilic clay, CaCl_2 brine and barite.

Apparatus and tests on Versaclean

Qualitative tests were made on the field-fluid Versaclean OBM samples, using a simple electrophoretic separating assembly shown schematically in Figure 1. The assembly had a container 21 for two parallel stainless steel plates 22 and the sample 23 to be tested. The plates were connected to a constant DC voltage supply of about 200 V, so that one electrode was negative and the other positive, and a field strength of about 1000 V/cm was generated. After a few minutes oil appeared close to the electrodes, and after about 20 min the assembly was dismantled. The negative electrode was coated with about 0.5 mm of deposit 24, the other remaining deposit-free but coated thinly with drilling fluid. With this arrangement of plates, the field was kept spatially-uniform by means of a guard electrode (not shown). Thus the presence of a uniformly-thick deposit over the negative electrode was evidence that deposition resulted from electrophoresis of positive particles, rather than dielectrophoresis which requires a field gradient.

An apparatus used for quantitative tests is shown schematically in Figure 2. The apparatus consisted of a cylindrical epoxy conductivity cell 25 of internal diameter about 20 mm, having three axially spaced annular carbon

electrodes 26. The electrodes were connected to a constant voltage supply so that the centre electrode was negatively charged and the other two were positively charged.

Versaclean was poured into this cell and a constant voltage applied. A layer of oil 27 was observed to form at the surface of the mud 28 and an electro-deposit 29 collected on the negative electrode. A barite layer 30 settled at the bottom of the cell. The oil is believed to rise to the surface owing to a weakening of the gel as fine particles migrated from the centre of the cell to form the deposit. The cell was weighed empty, and then after the treated drilling fluid (effluante) was poured out. The increment of weight comprised the weight of the deposit and the residual fluid unremoved by gravity that adhered to the inside of the cell. The API rheological parameters PV and YP, and the API 100 PSI fluid loss, were measured for the effluante poured from the cell.

The effect of voltage and time on the mass of the deposit is shown in Figure 3. Closed circles show the electrodeposit mass after 25 min. Open circles show the mass deposited after 40 minutes corrected to 25 min assuming the electrodeposit was directly proportional to the time of voltage application. The collected data show that the mass deposited was proportional to voltage and time.

A variety of different oil based drilling fluids were then investigated with the epoxy cell method, in which a voltage of 200 V was applied for a duration of 25 minutes. These fluids were two different field samples of Versaclean (Versaclean 1 and Versaclean 2), and a further sample of Versaclean 2 which has been centrifuged at 3000 rpm for 20 min

to remove barite. Measurements of the electrical stability and density of the untreated muds and of PV and YP before and after treatment are shown in Table 1.

Table 1: Properties of field and laboratory OBMs

	API Electrical Stability (untreated) (V)	Density (untreated) (g/ml)	PV (untreated)	PV (treated)	YP (untreated)	YP (treated)
Versaclean 1	517	1.45	78	69	37	32
Versaclean 2	435	1.455	58	52	30	25
Versaclean 2 Barite-free	449	1.025	39	32.5	28	27.5

- 5 Thus the PV and YP of all the Versaclean OBMs were reduced by the treatment.

Figure 4 shows a graph of the mass of the electrodeposit against voltage for each of the OBMs, including the Versaport OBM. This shows that the electrodeposit mass depends on the density of the mud, suggesting that the fine particles attracted to the negative electrode tend to trap the barite. The graph also shows that high voltages do not necessarily provide a greater electrodeposit. For all the field muds the electrodeposit mass reached a maximum between 450 to 500 V.

10 The collection process becomes less efficient as the applied voltage approached the breakdown voltage of the API Electrical Stability test (API 1988), possibly owing to a drop in the electric field experienced by the oil phase as chains of emulsion droplets begin to form prior to dielectric breakdown (Growcock et al. 1994).

15

20

Non-ohmicity and time-dependence

Using the apparatus of Figure 2 electrophoretic separation was performed on Versaclean OBM for various times and

voltages and the current measured. Figure 5 shows a graph of current against voltage. The current was observed to increase with voltage in typical ohmic behaviour up to 200 V but at higher voltages there was a clear non-ohmic and time-dependent behaviour. This suggests a complex conduction mechanism which corresponds with the observation that as the applied voltage approaches the breakdown voltage progressively less deposit is collected on the negative electrode. These results again suggest that the electrodeposition process is more effective at voltages less than the breakdown voltage of the API Electrical Stability test (API 1988).

In tests on Versaclean, the total solids content by weight in the deposit was found to be about 64%wt while that of the mud was 57%wt, showing that the deposit solids were more concentrated than in the drilling fluid. Similarly, the electrodeposit yield stress was about five times that of the untreated mud, suggesting that the deposit had more fine clay particles than the mud.

Measurements of the concentration by weight of metal species in the deposit and mud were made using inductively-coupled plasma metal analysis, and the results are shown in Table 2.

Table 2: Elemental analysis of deposit and mud

	Al/Ba	Al/Cl	Al/C	Al/Ca	Ba/C
Mud	0.185	0.356	0.025	0.207	0.136
Deposit	0.21	0.487	0.034	0.208	0.16
Deposit/mud % increase	15%	37%	36%	0%	18%

Assuming the clay to be the only source of Al, the ratios of Al to Ba, Cl and C suggest that the deposit has gained significantly in clay. The null change in Al/Ca suggests

that some Ca may be bonded to the clay, and the 18% increase in the Ba/C ratio shows that there was less oil in the deposit.

Effect of shear on field mud (Versaclean)

5 The effect of shear on the electrodeposition process was investigated using a modified Chan 35TM oilfield rheometer in which the outside of the rotor was electrically-isolated from the rheometer body and acted as one electrode, while a brass cup of inner diameter 57 mm was inserted into a heat cup to
10 act as the rheometer stator and also the other (earthed/grounded) electrode. In this configuration the drilling fluid could be sheared in the gap between the rotor and stator and the deposit could be collected on the outside of the rotor. The rotor gave a larger collection surface
15 area than the annular electrode of the epoxy cell of Fig. 2, while allowing the mud to be sheared and/or heated simultaneously with the electric field applied.

Using the Chan rotor R1 outer diameter of 40.65 mm and a brass cup inner diameter of 57.00 mm gave a laminar shear
20 rate per unit RPM at the surface of the rotor of 0.43 s⁻¹/RPM. The results are shown in Table 3. Some results are also plotted on Figure 6, which is a graph of deposit weight against rotor speed. Figure 6 demonstrates that the effect of shear was to reduce the amount of deposit.

Table 3: Effect of shear, voltage, and time on electrodeposit mass for field Versaclean OBM

Rotor speed (RPM)	Applied voltage (V)	Treatment time (min)	Deposit weight (g)	PV post-treatment	YP post-treatment
0	0	0	-	58	30
200	0	25	-	52	27
200	0	100	-	45.5	30
0	40	250	32.7	43	23
0	400	40	41.60	30	11
0	400	25	35.72	37	16
20	400	25	27.8	36	26
100	400	25	22.29	45	15
200	400	25	16.72	48	18
200	400	40	19.59	40	18
200	400	60	23.29	41	7

These results, together with a range of tests on samples of used field Versaclean OBM and lab Versaport OBM may be summarized as follows:

- With no shear, the longer the exposure to the electrical field, the greater the amount of deposit and the lower PV and YP.
- The deposit weight increases with both time and voltage in both static and sheared tests. The very low voltage test over a long time (40V at 250 min) produced a similar deposit to 400 V at 25 min.
- PV and YP were reduced as the deposit increased.
- Elemental analysis after treatment of the Versaport mud indicated that the electro-deposit was enriched in Ba, Ca, Al, Na, Cl and depleted in organics (C, H, N) compared to the original mud. The reverse was found in the treated mud, confirming solids-removal from the fluid.

- Shear reduced the mass of electro-deposit (see Figure 6) and the effect of electro-treatment on the rheology. Sheared electro-deposits were also more fluid than static electro-deposits.

- Combinations of static and sheared periods of electro-treatment generally increased the electro-deposit. The order of imposition of electric field and shear appears to have an effect on rheology.

- Reversal of the field polarity causes the deposit to detach from the electrode and slump to the bottom.

Other variations altering the sequence of electrical treatment and shear in two stages were attempted and the results are shown in Table 4. The mud was treated first for 25 min with an applied voltage of 400 V with no shear. Then the treated system was placed under a shear of 200 rpm for 25 min. The amount of deposit formed was higher and PV and YP was generally lower than that when the mud was subjected to a simultaneous electric field and shear. Reversing the order of this process resulted in a higher amount of material being deposited but also a higher PV and YP.

Table 4: Two phase test conditions and results of experiments investigating effect of a treatment combining shear and voltage on weight of deposit, PV and YP (Versaclean field-OBM)

Rotor speed (RPM)		Applied voltage (V)		Time (mn)		Deposit weight (g)	PV (treated)	YP (treated)
Phase 1	Phase 2	Phase 1	Phase 2	Phase 1	Phase 2			
0	200	400	0	25	25	27.27	22	20
200	0	0	400	25	25	31.58	44	21
200	200	0	400	25	25	17.49	43	20

Effect of temperature on field mud (Versaclean)

Figure 7 is a graph of deposit weight against test temperature obtained by testing the Versaclean OBM in the modified Chan rheometer. The effect of increasing the temperature, at a fixed voltage, was to usefully increase the weight of the deposit. Decreases in PV and YP, measured at laboratory temperature after treatment, are also shown in the graph.

Continuous-flow and batch embodiments

The experiments described above show the utility of treating oil based drilling or completion fluids with an electric field. We now propose continuous-flow and batch embodiments that may be useful in full-scale or engineering applications. These serve to demonstrate the application of the invention but other examples are possible.

Figure 8 shows schematically a longitudinal section through a continuous-flow device for recycling used OBM. The drilling or completion fluid 1 enters an electrically-conductive and horizontal pipe 2, which bifurcates into pipe 3 and 4, each branch containing a valve 5 and 6. A series of annular electrodes 7 are held in pipe 2 and insulated from it by means of insulators 8. Electrical contact to each annular electrode is made via leads 9 and insulating bushes 10. Leads 11 and 12 respectively connect the electrodes and the pipe 2 to an electrical supply. In operation electrodeposit 13 forms on each of electrodes 7.

We have found (see above) that shear tends to reduce the efficiency of the deposition process. However, Figure 6

shows that at sufficiently low shear rates, the efficiency is largely undiminished. For example, Figure 6 shows that 10 RPM had little effect on the deposition rate. In our modified Chan 35 oilfield rheometer, 10 RPM corresponds to about 4.3 s^{-1} . For a pipe of diameter D , the relation between wall shear rate (WSR), volumetric flow rate (Q) and mean axial velocity (V) is $\text{WSR} = 16V/(3D) = 64Q/(3\pi D^3)$. This sets an upper limit on V and Q , in order that the deposition process is not unduly lessened. For example, for $D = 0.1 \text{ m}$ and $\text{WSR} = 4.3 \text{ s}^{-1}$, $V = 0.22 \text{ m s}^{-1}$, approximately, which corresponds to about 100 l min^{-1} .

The device operates as follows. Deposit is collected on electrodes 7 with valve 5 open and valve 6 closed. Pipe 3 then exudes a drilling fluid with less fine particles than entered via pipe 2. After sufficient time (to be found by experiment and corresponding to a lessening deposition rate as the deposit intrudes into the body of pipe 2) valve 5 is closed, valve 6 is simultaneously opened, and the voltage applied to form the deposit is reversed. This pushes deposit into the body of pipe 2, where its greater density than the surrounding fluid causes it to be preferentially collected by pipe 4 and led into a suitable collection vessel.

An alternative continuous-flow embodiment for such a device is shown in longitudinal section in Figure 9a and in transverse section in Figure 9b. In this case the drilling or completion fluid 1' enters a horizontal pipe 2' which is an electrical insulator. Pipes 3' and 4', with valves 5' and 6', resemble the bifurcation and valves of the device shown in Figure 8. Electrodes 7' and 7'' now run axially along pipe 2', and are connected to a voltage source via leads 11'

and 12', such that the electro-deposit 13' collects along the lower electrode 7'' over a suitable time period and voltage, both to be determined by experiment. Pipe 3' then exudes a fluid with less fine particles than entered via pipe 2'.

5 After sufficient deposit is collected, the flow is stopped, valves 5' and 6' are closed and opened, respectively, the voltage is reversed, and the flow re-started. The re-start flow rate should be large enough to quickly remove the deposit, but not so large as to remix it with the incoming
10 fluid. The deposit then exudes via pipe 4' and led to a suitable collection vessel.

While the invention has been described in conjunction with the exemplary embodiments described above, many equivalent modifications and variations will be apparent to those
15 skilled in the art when given this disclosure. For example, in batch embodiments the electrodes may be set into a stirred or a static tank. Accordingly, the exemplary embodiments of the invention set forth above are considered to be illustrative and not limiting. Various changes to the
20 described embodiments may be made without departing from the spirit and scope of the invention.

References

American Petroleum Institute (1988) Recommended practice standard procedure for field testing drilling fluids. API, Recommended Practice 13B (RP 13B), 12th Ed., September 1, 5 1988.

Delgado AV (2002) Interfacial electrokinetics and electrophoresis. Marcel Dekker, New York.

Eow JS, Ghadiri M, Sharif AO, Williams TJ (2001) Electrostatic enhancement of coalescence of water droplets in 10 oil: a review of current understanding. Chem Eng J 84:173-192.

Growcock FB, Ellis CF, Schmidt DD (1994) Electrical stability, emulsion stability, and wettability of invert oil-based muds. SPE Drilling and Completion, March, 39-46.

15 Jones TB (1995) Electromechanics of particles. Cambridge University Press.

Pohl HA (1978) Dielectrophoresis. Cambridge University Press.

Thornton JD (1992) Science and practice of liquid-liquid extraction, Vol 1. Clarendon, Oxford.

Claims

1. A method of removing particulate solids from an oil based drilling or completion fluid, comprising:
exposing the fluid to an electric field to electrically
5 migrate particulate solids suspended therein, and
collecting the migrated particulate solids to remove them from the fluid.
2. A method according to claim 1, wherein the fluid comprises a water-in-oil emulsion, and the strength of the
10 electric field is lower than that required to coalesce the water droplets of the emulsion.
3. A method according to claim 1 or 2, wherein the strength of the electric field is less than 100,000 V/m.
4. A method according to any one of the previous claims,
15 wherein the strength of the electric field is greater than 10 V/m.
5. A method according to any one of the previous claims, wherein the PV and/or YP of the fluid are reduced as a result of the collection of the particulate solids.
- 20 6. A method according to any one of the previous claims, wherein the fluid contains clay particles.
7. A method according to any one of the previous claims, wherein the fluid contains weighting agent particles.
8. A method according to any one of the previous claims,
25 wherein the particulate solids in the fluid occupy at least 5 vol. % of the total fluid.

9. A method according to any one of the previous claims, wherein the fluid is a shear-thinning fluid which forms a gel when quiescent.

5 10. A method according to any one of the previous claims, further comprising heating the fluid to enhance the collection of particulate solids.

11. A method of recycling an oil based drilling or completion fluid by performing the method of any one of the previous claims.

10 12. A method according to claim 11, including the step of using a centrifuge or hydrocyclone to remove other particulate solids from the fluid.

ABSTRACT

A method of removing particulate solids from an oil based drilling or completion fluid is disclosed. The method involves exposing the fluid to an electric field to
5 electrically migrate particulate solids suspended therein, and collecting the migrated particulate solids to remove them from the fluid.

1/5

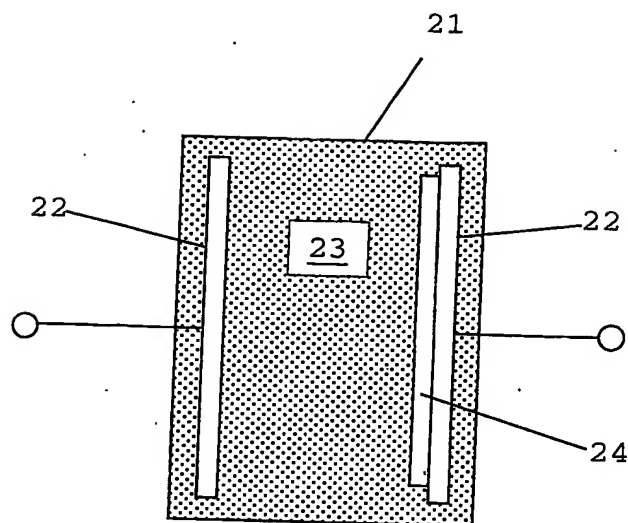


Figure 1

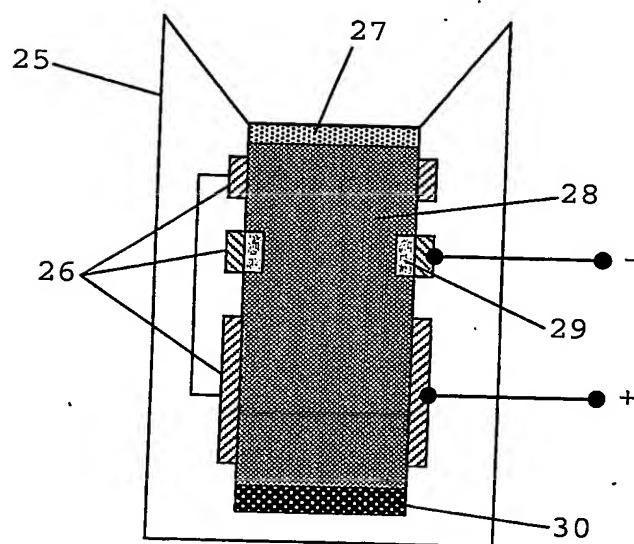


Figure 2

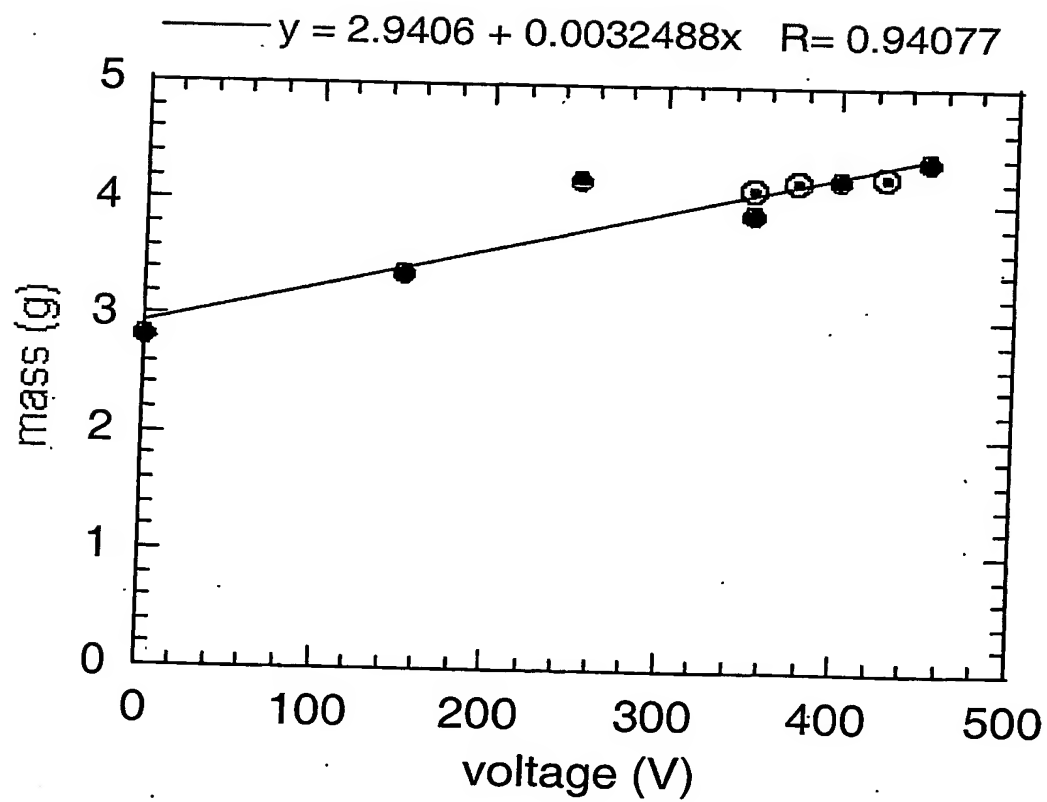


Figure 3

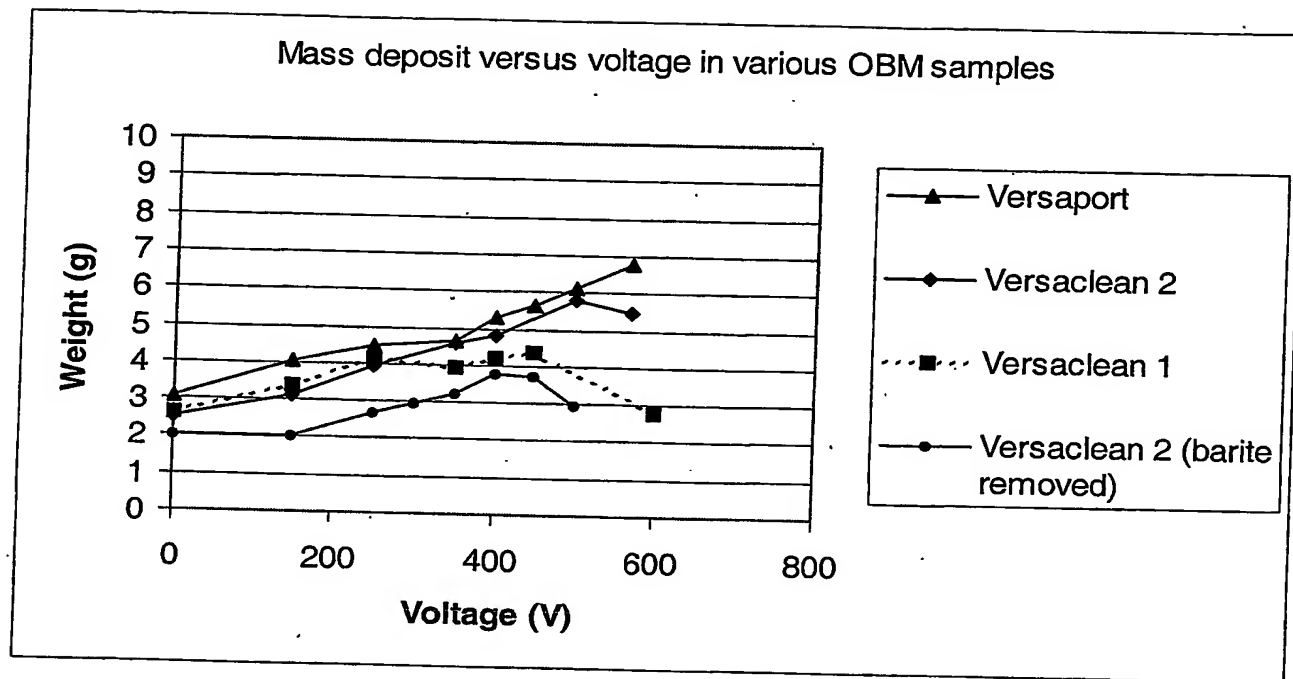


Figure 4

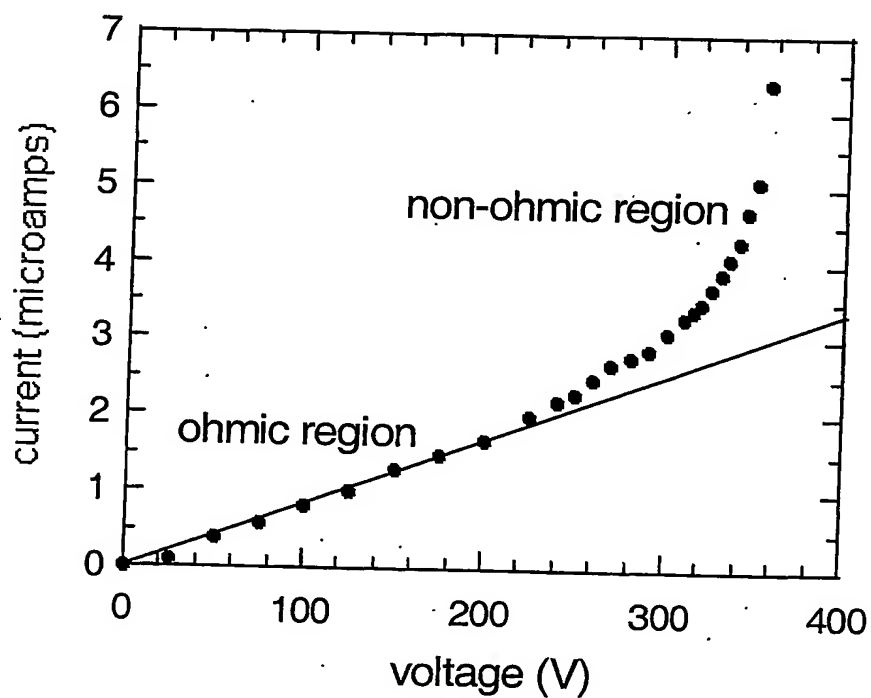


Figure 5

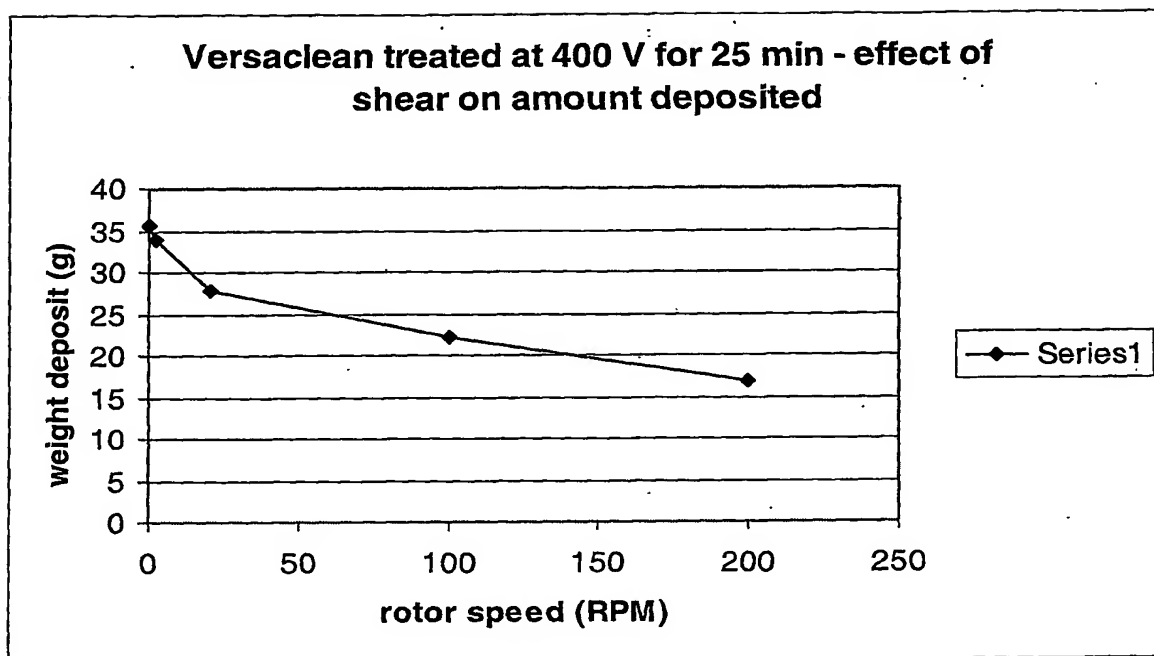


Figure 6

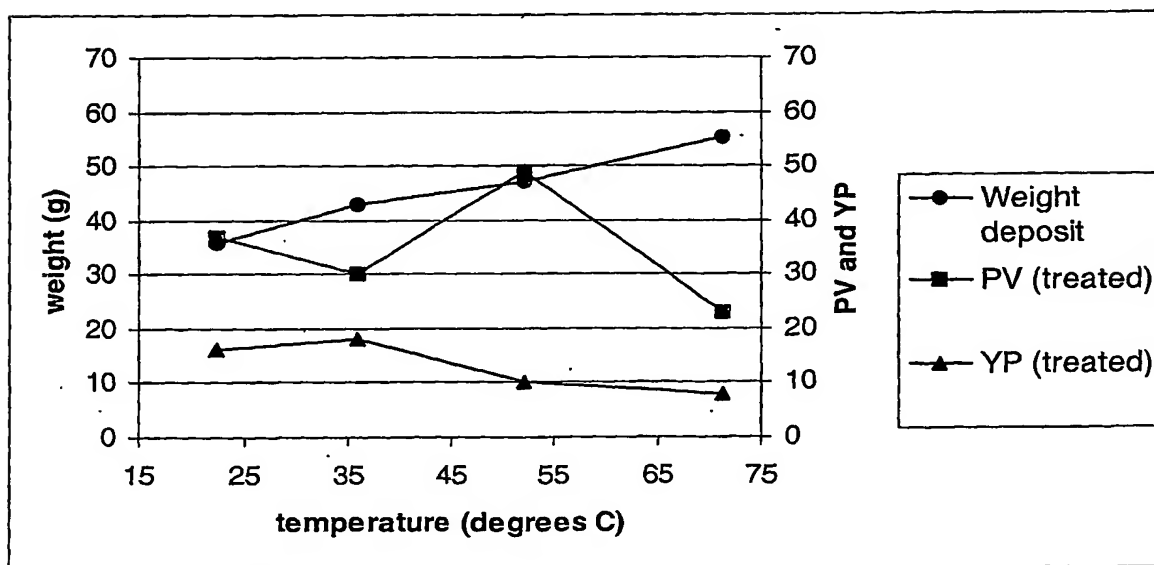


Figure 7

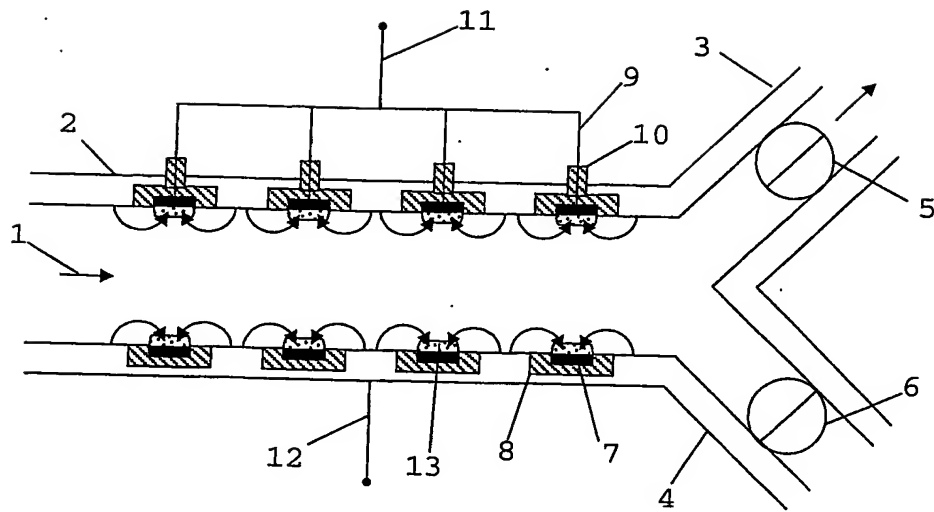


Figure 8

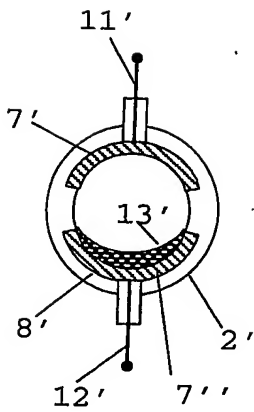


Figure 9(b)

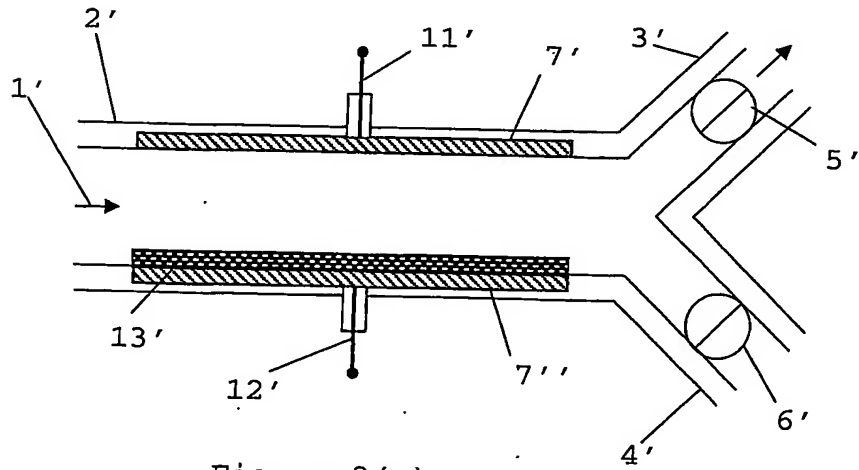


Figure 9(a)

PCT/GB2004/002863

